

D E C L A R A T I O N

I, Hideo KOSAKA, a national of Japan, c/o Sumitomo Chemical Intellectual Property Service, Limited, 5-33 Kitahama 4-chome Chuo-ku Osaka-shi, Osaka 541-8550, Japan, declare that to the best of my knowledge and belief the attached is a full, true and faithful translation into English made by me of the certified copy of Japanese Patent Application No. 2003-376589 attached thereto.

Signed this 12th day of June, 2008



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Hideo KOSAKA

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Inventor

Address or Domicile

[Inventor]

10 [Address] c/o 3-1-98, Kasugadenaka, Konohaka-ku, Osaka,  
Sumitomo Chemical Company, Limited

[Name] Masao YANAGAWA

[Inventor]

[Address] c/o 3-1-98, Kasugadenaka, Konohaka-ku, Osaka,  
15 Sumitomo Chemical Company, Limited

[Name] Kazunori IWAKURA

[Inventor]

[Address] c/o 3-1-98, Kasugadenaka, Konohaka-ku, Osaka,  
Sumitomo Chemical Company, Limited

20 [Name] Seiji ODA

[Applicant]

[Applicant's ID Number] 000002093

[Name] SUMITOMO CHEMICAL COMPANY, LIMITED

[Agent]

25 [Agent's ID Number] 100093285

[Patent Attorney]

[Name] Takashi KUBOYAMA

[Telephone] 06-6220-3405

[Elected Agent]

[Agent's ID Number] 100113000  
[Patent Attorney]  
[Name] Tohru NAKAYAMA  
[Telephone] 06-6220-3405

5 [Elected Agent]

[Agent's ID Number] 100119471  
[Patent Attorney]  
[Name] Masayuki ENOMOTO  
[Telephone] 06-6220-3405

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Document Name       SCOPE of CLAIMS

1. An olefin-trimerizing catalyst comprising

(A) a tantalum compound, and

(B) an organic metal compound, wherein the organic metal

5 compound (B) comprises at least one group selected from the group consisting of the following (1) to (5):

(1) a branched primary alkyl group having 4 to 15 carbon atoms,

10 (2) an aryl-substituted primary alkyl group having 7 to 15 carbon atoms,

(3) a homoalllyl group having 4 to 15 carbon atoms,

(4) a secondary alkyl group having 3 to 15 carbon atoms,

and

(5) a secondary alkenyl group having 4 to 15 carbon atoms.

15 2. The olefin-trimerization catalyst according to claim 1, wherein the tantalum compound (A) is a tantalum halide.

3. The olefin-trimerization catalyst according to claim 1 or 2, wherein the organic metal compound (B) comprises at least one group selected from the group consisting of isopropyl, 20 isobutyl, sec-butyl, homo-allyl, cyclopentylmethyl, cyclohexylmethyl, 1-phenethyl, and 2-phenethyl groups.

4. The olefin-trimerizing catalyst according to claim 1 or 2, wherein the organic metal compound (B) comprises isobutyl group.

25 5. The olefin-trimerizing catalyst according to claim 1 or 2, wherein the organic metal compound (B) is an isopropylmagnesium halide, an isobutylmagnesium halide, a sec-butylmagnesium halide, a cyclopentylmagnesium halide, a cyclohexylmagnesium halide, a 1-phenethylmagnesium halide, a

2-phenethylmagnesium halide, isopropyllithium,  
isobutyllithium, sec-butyllithium, cyclopentyllithium,  
cyclohexyllithium, 1-phenethylithium, 2-phenethylithium,  
triisopropylaluminum, triisobutylaluminum,

5 tri-sec-butylaluminum, tricyclohexylaluminum,  
isobutylaluminum dichloride, diisobutylaluminum chloride, a  
diisobutylaluminum halide, a modified methylaluminoxane,  
isobutylaluminoxane, tetraisopropyltin,  
isopropyltrimethyltin, tetraisobutyltin or a diisobutyltin  
10 dihalide.

6. The olefin-trimerizing catalyst according to claim  
1 or 2, wherein the organic metal compound (B) is  
triisobutylaluminum, a modified methylaluminoxane, or  
isobutylaluminoxane.

15 7. The olefin-trimerizing catalyst according to any one  
of claims 1 to 6, wherein the amount of the organic metal compound  
(B) is from 0.5 to 3 moles in terms of the alkyl group(s) per  
mole of the tantalum compound (A).

20 8. The olefin-trimerizing catalyst according to any one  
of claims 1 to 7, wherein the olefin is ethylene.

9. The catalyst according to any one of claims 1 to 8,  
which is obtained by contacting the tantalum compound (A) with  
the organic metal compound (B).

25 10. An olefin-trimerizing process, which comprises  
trimerizing an olefin in the presence of the catalyst according  
to any one of claims 1 to 9.

11. The olefin-trimerizing process according to claim  
10, which is carried out at an absolute pressure of from normal  
pressure to a pressurized pressure.

12. The olefin-trimerizing process according to claim 11, wherein the absolute pressure is from normal pressure to 30 MPa.

13. The olefin-trimerizing process according to any one of claims 10 to 12, which is carried out at a temperature of 150°C or lower.

14. The olefin-trimerizing process according to claim 13, which is carried out at a temperature of 10 to 80°C.

15. The olefin-trimerizing process according to any one of claims 10 to 14, which is carried out in the presence of a solvent.

16. The olefin-trimerizing process according to claim 15, wherein the solvent is an aromatic compound.

17. The olefin-trimerizing process according to claim 15, wherein the solvent is at least one selected from the group consisting of benzene, toluene, xylene, chlorobenzene and dichlorobenzene.

18. The olefin-trimerizing process according to any one of claims 10 to 17, wherein the olefin is ethylene.

[Document Name] Specification

[Title of the Invention]

Olefin-trimerizing catalyst and a method of  
olefin-trimerization using the same

5 [Technical Field]

[0001]

The present invention relates to a trimerization catalyst  
for olefin, and a process for trimerizing an olefin using the  
catalyst. More specifically, the present invention relates to  
10 an olefin-trimerizing catalyst containing tantalum compound and  
an organic metal compound as alkylating agent, which enables  
high catalytic activity, and an olefin-trimerizing method using  
the same.

[Background Art]

15 [0002]

As a process of using a tantalum compound to selectively  
trimerize an olefin, in particular, ethylene, there are disclosed  
in Patent Literature 1 and Non-patent Literature 1 a catalyst  
composition comprising a tantalum compound and an alkylating  
20 agent. As the alkylating agent, disclosed are tetramethyltin,  
tetraethyltin, allyltriphenyltin, tetra-n-butyltin,  
tetraphenyltin, dimethylzinc, diethylzinc, trimethylaluminum,  
triethylaluminum, methylaluminoxane, dimethylaluminum  
chloride, methyl lithium, n-butyllithium, tert-butyllithium,  
25 phenyllithium, methylmagnesium bromide, and the like. However,  
the ethylene-trimerizing process using the catalyst composition  
disclosed in the above-mentioned documents has a problem in that  
the catalytic activity thereof is not necessarily sufficient.

[0003]



[Patent Literature 1] US6344594

[Non-patent Literature] J. Am.chem.. Soc., 2001, 123, 7423

[Disclosure of the Invention]

[Problems to be Solved by the Invention]

5 [0004]

Under the circumstances, the problems to be solved by the invention is to provide an olefin-trimerizing catalyst containing tantalum compound and an organic metal compound as alkylating agent, which enables high catalytic activity, and  
10 an olefin-trimerizing method using the same.

[Means for Solving the Problems]

[0005]

That is, the first invention relates to an olefin-trimerizing catalyst comprising  
15 (A) a tantalum compound, and  
(B) an organic metal compound, wherein the organic metal compound (B) comprises at least one group selected from the group consisting of the following (1) to (5):

(1) a branched primary alkyl group having 4 to 15 carbon  
20 atoms,

(2) an aryl-substituted primary alkyl group having 7 to 15 carbon atoms,

(3) a homo-allyl group having 4 to 15 carbon atoms,

(4) a secondary alkyl group having 3 to 15 carbon atoms ,  
25 and

(5) a secondary alkenyl group having 4 to 15 carbon atoms;  
and a process for trimerizing an olefin in the presence of the above-mentioned olefin-trimerizing catalyst.

[Effect of the Invention]

[0006]

According to the invention, there is provided an olefin-trimerizing catalyst containing tantalum compound and an organic metal compound as alkylating agent, which enables high catalytic activity, and an olefin-trimerizing method using the same. 1-Hexene, which is a useful raw material co-monomer for the production of LLDPE, can be produced efficiently and with high selectivity by using ethylene as raw material.

[Best Mode for Carrying Out the Invention]

10 [0007]

The tantalum compound (A) in the invention includes a tantalum halide, a tantalum alkoxide, and the like. Preferred is a tantalum halide, and is more preferably tantalum (V) fluoride, tantalum (V) chloride, tantalum (V) bromide, tantalum (V) iodide, and the like.

[0008]

The organic metal compound (B) comprises at least one group selected from the group consisting of the following (1) to (5):

(1) a branched primary alkyl group having 4 to 15 carbon atoms,

(2) an aryl-substituted primary alkyl group having 7 to 15 carbon atoms,

(3) a homo-allyl group having 4 to 15 carbon atoms,

(4) a secondary alkyl group having 3 to 15 carbon atoms, and

(5) a secondary alkenyl group having 4 to 15 carbon atoms.

[0009]

(1) Specific examples of the branched primary alkyl group having 4 to 15 carbon atoms include isobutyl, 2-methylbutyl,

2-ethylbutyl, 2,2-dimethylpropyl, isopentyl, 2-methylpentyl, isohexyl, 2-methylhexyl, 2-ethylhexyl, cyclopentylmethyl, and cyclohexylmethyl groups. Preferred are isobutyl, 2-methylbutyl, 2-methylpentyl, cyclopentylmethyl, and  
5 cyclohexylmethyl groups. More preferred is isobutyl group.

[0010]

(2) Specific examples of the aryl-substituted primary alkyl group having 7 to 15 carbon atoms include benzyl, 2-phenylethyl, and 2-phenylpropyl groups. Preferred is the  
10 2-phenylethyl group.

[0011]

(3) Specific examples of the homo-allyl group having 4 to 15 carbon atoms include 3-butenyl, 2-methyl-3-butenyl, and 3-methyl-3-butenyl groups. Preferred is 3-butenyl group.

15 [0012]

(4) Specific examples of the a secondary alkyl group having 3 to 15 carbon atoms include isopropyl, sec-butyl, 2-(3-methyl)-butyl, 2-pentyl, cyclopentyl, cyclohexyl, and 1-phenylethyl groups. Preferred are the isopropyl, sec-butyl, 20 cyclopropyl, cyclopentyl, cyclohexyl, and 1-phenylethyl groups.

[0013]

(5) Specific examples of the secondary alkenyl group having 4 to 15 carbon atoms include 1-methyl-2-propenyl, 3-(1-pentenyl), 25 3-(4-methyl-1-pentenyl), and 1,2-dimethyl-2-propenyl groups. Preferred is the 1-methyl-2-propenyl group.

[0014]

Of the above, the following are more preferred, as the organic metal compound (B), those comprising at least one group

selected from the group consisting of isopropyl, isobutyl, sec-butyl, 3-butenyl, cyclopentylmethyl, cyclohexylmethyl, 1-phenylethyl, and 2-phenylethyl groups. Most preferred is a compound comprising isobutyl group.

5 [0015]

The organic metal compound (B) in the invention are supposed to act as an alkylating agent. "Alkylating agents" hereinafter mean the organic metal compound (B).

[0016]

10 Specific examples of the organic metal compound (B) include, for example, alkyl lithium having the alkyl groups as described above, alkylmagnesium halides, alkylaluminum, alkylaluminum oxane, and alkyltin.

[0017]

15 Specific examples of the alkyl lithium include isopropyl lithium, sec-butyllithium, isobutyllithium, cyclopentyl lithium, 2,2-dimethylpropyl lithium, cyclohexyl lithium, 1-phenylethyl lithium, and 2-phenylethyl lithium. Preferred are isopropyl lithium, sec-butyllithium, isobutyllithium and  
20 the like.

[0018]

Specific examples of the alkylmagnesium halides include isopropylmagnesium halides, cyclopentylmagnesium halides, 2,2-dimethylpropylmagnesium halides, cyclohexyl halides,  
25 1-methyl-2-propenylmagnesium halides, 2-phenylethylmagnesium halides, 3-butenylmagnesium halides, cyclopropylmagnesium halides, sec-butylmagnesium halides, isobutylmagnesium halides, 2-ethylhexylmagnesium halides, and 2-ethylbutylmagnesium halides. Preferred are isopropylmagnesium halides,

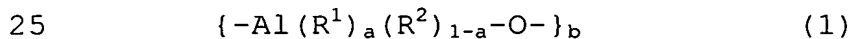
cyclopentylmagnesium halides, cyclohexylhalides,  
2-phenylethylmagnesium halides, 3-butenylmagnesium halides,  
sec-butylmagnesium halides, isobutylmagnesium halides and the  
like. Preferred are the isopropylmagnesium halides,  
5 sec-butylmagnesium halides, and isobutylmagnesium halides.  
Examples of the halides in the alkylmagnesium halides above  
include chlorine, bromine, iodine and the like.

[0019]

Specific examples of the alkylaluminum include  
10 triisopropylaluminum, triisobutylaluminum,  
tri-sec-butylaluminum, tricyclopentylaluminum,  
tri(2,2-dimethylpropyl)aluminum, tricyclohexylaluminum,  
diisopropylaluminum chloride, isopropylaluminum dichloride,  
diisobutylaluminum chloride, isobutylaluminum dichloride,  
15 di-sec-butylaluminum chloride, sec-butylaluminum dichloride,  
and diisobutylaluminum hydride. Preferred are  
triisopropylaluminum, triisobutylaluminum,  
tri-sec-butylaluminum, diisobutylaluminum chloride,  
isobutylaluminum dichloride, and diisobutylaluminum hydride.  
20 More preferred is triisobutylaluminum.

[0020]

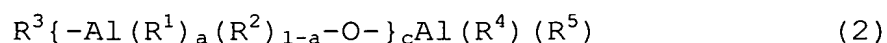
Examples of the alkylaluminumoxane include  
cyclic aluminumoxane having a structure represented by the  
following formula (1):



wherein  $R^1$  represents a hydrogen atom or a hydrocarbon having  
1 to 8 carbon atoms,  $R^2$  represents a branched primary alkyl group  
having 4 to 15 carbon atoms, an aryl-substituted primary alkyl  
group having 7 to 15 carbon atoms, a homo-allyl group which has

4 to 15 carbon atoms, a secondary alkyl group which has 3 to 15 carbon atoms, or a secondary alkenyl group which has 4 to 15 carbon atoms, a represents an numerical value of 0 or more and less than 1, and b represents an integer of 2 or more; or

5 linear aluminoxane having a structure represented by the formula (2):



wherein  $R^1$ ,  $R^2$  and a have the same meanings as described above,  $R^3$ ,  $R^4$  and  $R^5$ , which may be the same or different, each represents  
10 a hydrogen atom, or a hydrocarbon group having 1 to 8 carbon atoms, and c represents an integer of 1 or more.

[0021]

Specific examples of the hydrocarbon having 1 to 8 carbon atoms for  $R^1$ ,  $R^3$ ,  $R^4$  or  $R^5$  include methyl, ethyl, n-propyl,  
15 isopropyl, n-butyl, sec-butyl, isobutyl and tert-butyl groups. Preferred are the methyl, and isobutyl groups.

In  $R^2$ , specific examples of the branched primary alkyl group having 4 to 15 carbon atoms, the aryl-substituted primary alkyl group having 7 to 15 carbon atoms, the homo-allyl group  
20 having 4 to 15 carbon atoms, the secondary alkyl group having 3 to 15 carbon atoms, or the secondary alkenyl group having 4 to 15 carbon atoms, include the substituents described above. Preferred is isobutyl group. "a" represents a numerical value of 0 or more and less than 1. "b" is an integer of 2 or more,  
25 and "c" represents an integer of 1 or more. Preferably, b is an integer of 2 to 40 and c is an integer of 1 to 40.

[0022]

Specific examples of the aluminoxane include a modified methylaluminoxane (aluminoxane wherein methyl groups in

methyraluminoxane are partially substituted with isobutyl groups), and isobutylaluminoxane.

[0023]

The above-mentioned aluminoxane can be produced by various methods which are not particularly limited. The aluminoxane can be produced in accordance with a known method. For example, the aluminoxane can be produced by bringing water into contact with a solution in which a trialkylaluminum (such as triisobutylaluminum) is dissolved in a suitable organic solvent (such as benzene or an aliphatic hydrocarbon). Furthermore, exemplified is a method of bringing a trialkylaluminum (such as triisobutylaluminum) into contact with a metal salt containing crystal water (such as copper sulfate hydrate). A commercially available product may be used.

[0024]

Specific examples of the alkyltin include tetraisopropyltin, isopropyltrimethyltin, tetraisobutyltin, tetra(2,2-dimethylpropyl)tin, diisobutyltin dichloride, tetra-sec-butyltin, and tetracyclohexyltin. Preferred are tetraisopropyltin, tetraisobutyltin, tetra-sec-butyltin, and the like.

[0025]

The above-mentioned alkylating agents may be used alone or in the form of a mixture of two or more thereof.

[0026]

The olefin-trimerizing catalyst of the invention, which comprises a tantalum compound and an alkylating agent, can be prepared by bringing the tantalum compound and the alkylating agent into contact with each other. The method for the

preparation is not particularly limited. For example, the catalyst can be prepared by bringing the tantalum compound and the alkylating agent into contact with each other in a solvent, or by contacting them with each other without using any solvent, and then adding a solvent to the resultant. The contact of the tantalum compound with the alkylating agent is beforehand conducted, and subsequently the mixture is brought into contact with an olefin, whereby the trimerization can be carried out. The contact of the tantalum compound with the alkylating agent can be conducted in the presence of an olefin, whereby the trimerizing reaction can be started at the same time when the tantalum compound is brought into contact with the alkylating agent. The mixing order of these starting materials is not particularly limited. Preferably, the alkylating agent is added to the tantalum compound.

[0027]

In the preparation of the catalyst of the invention and the trimerizing reaction, a solvent is used. Examples of the solvent used herein include aliphatic hydrocarbons such as butane, pentane, hexane, heptane, octane, isooctane, cyclopentane, methylcyclopentane, cyclohexane, methylcyclohexane, cyclooctane, and decalin; aromatic hydrocarbons such as benzene, toluene, xylene, cumene, ethylbenzene, monochlorobenzene, or dichlorobenzene; and halogenated hydrocarbons such as dichloromethane, chloroform, carbon tetrachloride, or dichloroethane. The olefin itself which is the starting material for the trimerizing reaction, or a reaction product olefin such as 1-butene, hexene, octene, or the like can be used as the solvent.



[0028]

The solvent is preferably an aromatic hydrocarbon, and is more preferably benzene, toluene, xylene, or the like. These solvents may be used alone or in the form of a mixture  
5 of two or more thereof.

[0029]

The concentration of the tantalum compound when the catalyst of the invention is prepared is not particularly limited, and is usually from 0.0001  $\mu\text{mol}$  to 100 mmol, preferably from  
10 0.001  $\mu\text{mol}$  to 10 mmol.

[0030]

In the catalyst of the invention, the amount of the alkylating agent is usually from 0.5 to 4 moles, preferably from 0.7 to 3 moles, more preferably from 1 to 2.5 moles in terms  
15 of the alkyl group(s) per mol of the tantalum compound. The wording "in terms of the alkyl group(s)" means that a number corresponding to the mole number of the alkyl group(s) which can react with the tantalum compound, and can be represented as the product of the mole number of the alkylating agent per  
20 mol of the tantalum compound and the number of the alkyl group(s) that the alkylating agent has. For example, when the amount of isopropyllithium is 1 mole per mol of the tantalum compound, the amount in terms of the alkyl group(s) is 1 mole. When the amount of diisopropylzinc is 1 mole per mol of the compound,  
25 the amount in terms of the alkyl group(s) is 2 moles.

[0031]

The temperature when the catalyst of the invention is prepared is usually from -100 to 250°C, preferably from -78 to 150°C. The time for the preparation is not particularly limited,

and is usually from 0 minute to 24 hours.

The preparation of the catalyst of the invention and the trimerizing reaction are preferably conducted in an inert gas atmosphere while the contact with water is avoided. Thus, it  
5 is preferred that the compounds to be used are sufficiently dried in advance.

[0032]

The thus-prepared catalyst is used to carry out the trimerizing reaction of an olefin. The amount of the catalyst  
10 of the invention is not particularly limited, and is usually from 0.001  $\mu\text{mol}$  to 100 mmol, preferably from 0.01  $\mu\text{mol}$  to 10 mmol per liter of the solvent.

[0033]

Examples of the olefin which is used as the starting  
15 material in the invention include  $\alpha$ -olefins such as ethylene, propylene, 1-butene, 1-pentene, 1-hexene, 1-heptene, 1-octene, 1-nonene, or 1-decene; internal olefins such as 2-butene, 2-pentene, 2-hexene, 3-hexene, 2-octene, 3-octene, and 4-octene; branched olefins such as isobutylene,  
20 3-methyl-1-butene, 4-methyl-1-pentene, or 2-ethyl-1-hexene; and diolefins such as 1,3-butadiene, isoprene, 1,4-pentadiene, or 1,5-hexadiene.

[0034]

The catalyst of the present reaction is highly active and  
25 particularly suitable for the trimerizing reaction of ethylene, and makes it possible to yield 1-hexene with a high activity and a high selectivity.

[0035]

The temperature of the trimerizing reaction in the

invention is usually from -100 to 250°C, preferably 150°C or lower, more preferably from 0 to 200°C, even more preferably from 10 to 80°C. The reaction pressure is usually an absolute pressure of from normal pressure to a pressurized pressure, preferably of from 0 to 300 MPa, more preferably of from 0 to 30 MPa. The reaction time is not particularly limited, and is usually from 0 minute to 24 hours.

[0036]

The starting material olefin may be continuously supplied to keep the above-mentioned pressure, or may be sealed up at the above-mentioned pressure as the reaction is started. The olefin diluted with nitrogen, argon, helium or the like may be used.

[0037]

The present reaction can be carried out in a batch-wise manner, semi-continuous manner, or continuous manner. After the end of the reaction, an inactivating agent such as water, an alcohol, hydrochloric acid, or an aqueous sodium hydroxide solution, is added to the reaction solution, thereby terminating the reaction. After completion of the reaction, the inactivated catalyst is removed by a known demineralization treatment such as extraction with water or an aqueous alkaline solution. Thereafter, the desired olefin can be separated by a known operation such as distillation or extraction.

[0038]

The trimerizing reaction of an olefin is preferably carried out under a reaction condition wherein the water content in the reaction system is 50 moles or less per mole of the tantalum atom and the amount of molecular oxygen in the reaction system

is 10 moles or less per mole of the tantalum atom.

#### Examples

[0039]

The present invention will be illustrated in more detail  
5 by way of the following examples. However, the invention is  
not limited to these examples.

[0040]

#### Example 1

Toluene was charged into an autoclave in the atmosphere  
10 of nitrogen, and the temperature was maintained at 40°C, and  
then ethylene was charged at a pressure of 0.6 Mpa and  
stabilized. Thereto was added 0.8 mL of a solution of 22.4 mg  
of tantalum pentachloride dissolved in 10 mL of toluene (the  
amount of tantalum pentachloride: 5  $\mu$ mol). Thereinto was  
15 charged 13  $\mu$ L (3.3  $\mu$ mol) of triisobutylaluminum (manufactured  
by Tosoh Fine Chemicals Pte Ltd., 0.25 mol/L solution in toluene),  
and reacted for a time shown in Table 1. The reaction container  
was cooled to room temperature, and next the pressure was returned  
to normal pressure. The reaction solution was analyzed by gas  
20 chromatography. A solid matter contained in the reaction  
solution was filtrated off with filter paper. This solid was  
air-dried and then dried at a reduced pressure. The weight  
thereof was then measured. The results are shown in Table 1.

[0041]

#### 25 Example 2

The reaction operations were carried out in a similar  
manner as in Example 1 except using the kind of an alkylating  
agent, a charged amount thereof and a reaction time shown in  
Table 1. The results are shown in Table 1. PBAO represents

polyisobutylaluminumoxane.

[0042]

Table 1

Examples	1	2
TaCl <sub>5</sub> : $\mu$ mol	5.0	5.0
Alkylating agent $\mu$ mol	TIBA 3.3	PBAO 10.0
Reaction time: hour(s)	0.44	1.5
Reaction temperature: °C	40	40
Components: wt%		
C4	10.3 (99.0)	3.4 (91.2)
C6	84.2 (99.0)	95.4 (98.7)
C8	0.9 (0)	0.0
C10	3.7 (0)	1.2 (0)
C12	0.0	0.0
C14	0.2 (0)	0.0
C16	0.0	0.0
Solid component (PE)	0.7	0.0
Activity: mol/(mol(cat.)-hr)		
1-Butene	190	9
1-Hexene	1034	176
1-Octene	0	0
1-Decene	0	0
1-Dodecene	0	0
1-Tetradecene	0	0
1-Hexadecene	0	0

C4: Butene, C6: Hexene, C8: Octene, C10: Decene, C12: Dodecene,

5 C14: Tetradecene, C16: Hexadecene

The number in parentheses in each column for the components represents the purity of linear  $\alpha$ -olefins in the each of the components ((the amount of linear  $\alpha$ -olefins/the total amount of isomers of each of the components)  $\times 100$ )

10 TIBA: Triisobutylaluminum

PBAO: Polyisobutylaluminumoxane (manufactured by Tosoh Fine Chemicals Pte Ltd.)

[0043]

### Example 3

Toluene was charged into an autoclave in the atmosphere of nitrogen, and the temperature was maintained at 40°C, and then ethylene was charged at a pressure of 0.6 Mpa and stabilized. Thereto was added 0.8 mL of a solution of 167.9 mg of tantalum pentachloride suspended in 15 mL of toluene (the amount of tantalum pentachloride: 25  $\mu$ mol). The temperature thereof was then stabilized at 40°C, and charged 26  $\mu$ L (50  $\mu$ mol) of MMAO-3A (modified methylaluminoxane manufactured by Tosoh Fine Chemicals Pte Ltd., 1.9 mol/L solution in toluene), and reacted for 0.2 hour. The reaction container was cooled to room temperature, and next the pressure was returned to normal pressure. The reaction solution was analyzed by gas chromatography. A solid matter contained in the reaction solution was filtrated off with filter paper. This solid was air-dried and then dried at a reduced pressure. The weight thereof was then measured. The results are shown in Table 2.

[0044]

### Comparative Example 1

The same operations as in Example 3 were carried out except that dimethylzinc was used instead of MMAO-3A and the reaction was conducted for a reaction time shown in Table 2. The results are shown in Table 2.

[0042]

Table 2

	Example 3	Comparative Example 1
TaCl <sub>5</sub> : $\mu$ mol	25	25
Alkylating agent $\mu$ mol	MMAO-3A 50	ZnMe <sub>2</sub> 25
Reaction time: hour(s)	0.2	1.3

Reaction temperature: °C	40	40
Components: wt%		
C4	3.3 (100)	12.3 (98.4)
C6	87.4 (97.4)	76.4 (86.9)
C8	3.1 (3.2)	1.9 (0)
C10	6.2 (0)	3.4 (0)
C12	0.6 (16.7)	0.2 (0)
C14	1.2 (0)	0.0
C16	0.0	0.0
Solid component (PE)	1.4	0.0
Activity: mol/(mol(cat.)-hr)		
1-Butene	33	12
1-Hexene	568	42
1-Octene	0	0
1-Decene	0	0
1-Dodecene	0	0
1-Tetradecene	0	0
1-Hexadecene	0	0

C4: Butene, C6: Hexene, C8: Octene, C10: Decene, C12: Dodecene, C14: Tetradecene, C16: Hexadecene

The number in parentheses in each column for the components represents the purity of linear  $\alpha$ -olefins in the each of the components ((the amount of linear  $\alpha$ -olefins/the total amount of isomers of each of the components)  $\times$  100)

MMAO-3A: Modified methylaluminoxane (manufactured by Tosoh Fine Chemicals Ltd.)

[Document Name]                      Abstract

[Summary]

[Problems] The present invention provides an olefin-trimerizing catalyst containing tantalum compound and an organic metal compound as alkylating agent, which enables high catalytic activity, and an olefin-trimerizing method using the same.

Means for Solving the problem

[Means for Solving] An olefin-trimerization catalyst comprising

(A) a tantalum compound, and

(B) an organic metal compound,

wherein the organic metal compound (B) comprises at least one group selected from the group consisting of the following (1) to (5):

(1) a branched primary alkyl group having 4 to 15 carbon atoms,

(2) an aryl-substituted primary alkyl group having 7 to 15 carbon atoms,

(3) a homoallyl group having 4 to 15 carbon atoms,

(4) a secondary alkyl group having 3 to 15 carbon atoms,

and

(5) a secondary alkenyl group having 4 to 15 carbon atoms.

[Selected Drawings]    None